

Homework #11

- (10 pts) Water drains from a large tank through a system made of $D = 0.2\text{ m}$ inner diameter pipe having a surface roughness of $\varepsilon = 0.00026\text{ m}$ (Fig. 1). Discharge to the atmosphere is $H = 4.5\text{ m}$ below the free surface and the volume flow rate is $Q = 0.05\text{ m}^3/\text{s}$. If the four right-angle pipe components each have a loss coefficient of $K_a = 0.25$ and the exit itself has a loss coefficient of $K_e = 1$, calculate the total length of the straight pipe sections. (We assume that the inlet to the pipe is “well-rounded” so that its losses are negligible.) Assume a water viscosity and density of $\nu = 1.2 \times 10^{-6}\text{ m}^2/\text{s}$ and $\rho = 1000\text{ kg}/\text{m}^3$, respectively.

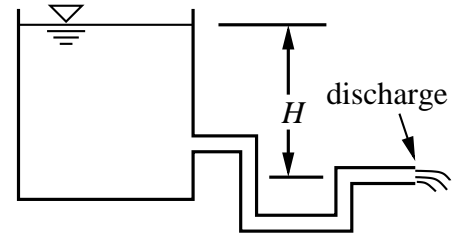


Fig. 1: Piping system.

- (10 pts) A water company is considering replacing a long section of a very old 0.5 m inner diameter “main”. This pipe has a relative roughness of $\varepsilon/D = 0.02$. One option is to dig the whole system up, but this would be very expensive. A junior engineer suggests pushing a hydrodynamically smooth plastic liner of inner diameter 0.4 m through the old pipe instead. Although this would be much cheaper, this new configuration would still need to carry the same volume flow rate $Q = 1\text{ m}^3/\text{s}$ as the older, larger pipe. If there is to be no net increase in pressure drop, will this approach work? Assume a water viscosity of $\nu = 1.2 \times 10^{-6}\text{ m}^2/\text{s}$.

- (10 pts) A pump moves water into a very large tank at a flow rate of $Q = 0.01\text{ m}^3/\text{s}$ through $L = 100\text{ m}$ of hydrodynamically smooth pipe (Fig. 2, not shown to scale). The pipe is horizontal and has an inner diameter of $D = 0.075\text{ m}$. At the instant shown, there is an $h = 10\text{ m}$ -deep column of water already in the tank. What pressure, P_p , must the pump step the flow up to at its outlet? Assume $\nu = 1 \times 10^{-6}\text{ m}^2/\text{s}$ and $\rho = 1000\text{ kg}/\text{m}^3$ and that the viscous losses due to the flow entering the tank are characterized by the loss coefficient $K = 1$.

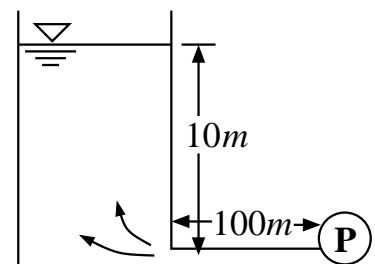


Fig. 2: Pumping water.

- (10 pts) Oil flows steadily in a horizontal pipe of constant diameter $D_1 = 0.2\text{ m}$ at an average velocity of $\bar{u}_1 = 1\text{ m}/\text{s}$ (Fig. 3). Oil viscosity is $\nu = 0.001\text{ m}^2/\text{s}$ and the flow is fully-developed. The flow eventually reaches a smooth contraction and enters into a smaller pipe of diameter $D_2 = 0.1\text{ m}$, quickly becoming fully developed. Determine the respective friction factors f_1 and f_2 in the larger and smaller pipes.

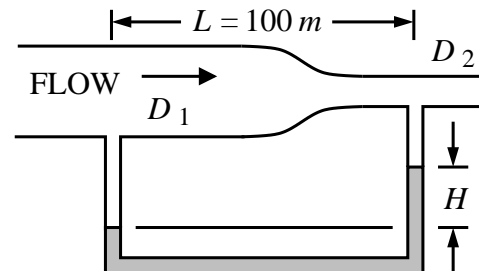


Fig. 3: Oil flow in a pipe.

- (10 pts) The configuration in Question 4 is exactly horizontal and two static ports are separated by $L = 100\text{ m}$, as measured along the pipe. These ports are connected by a liquid

mercury manometer (also shown in Fig. 3), whose fluid density is $\rho_m = 13500 \text{ kg/m}^3$. Here, the contraction is halfway between the static ports and is very short compared to the overall length of $L = 100 \text{ m}$. Therefore, taking as a first approximation that f_1 applies over the first 50 m of pipe length and f_2 applies over the subsequent 50 m of length, determine the manometer reading, H . Gravitational acceleration is $g = 9.8 \text{ m/s}^2$ and oil density is $\rho_o = 900 \text{ kg/m}^3$. From a design perspective, comment whether this manometer configuration would be a good method for measuring pressure drop.